

A Comparative Study of BOD Rate Constant of Two Waste Water Samples

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ABSTRACT: *The BOD (Biochemical Oxygen Demand) is the amount of oxygen (O_2) in mg/lit or ppm (parts per million) to oxidize biodegradable organic waste by microorganisms aerobically. The reaction kinetics involved in degradation process of the biodegradable organic matter with the help of microorganisms in the presence of dissolved oxygen (DO) and rejuvenation of the same in any water body may be first order or half order or second order or combination of them. Assuming the first order one, a comparative study has been envisioned between the BOD rate constants K_1 of two waste-water samples, collected from two different sources in a municipality area. Simultaneously, the other parameters e.g. pH, temperature, TSS, COD of the two waste water samples were determined using standard method to ascertain the characteristic features of the same.*

KEYWORDS: *Municipal waste water, physico-chemical parameters, BOD- rate constant, waste water treatment.*

1. INTRODUCTION:

Water is essential for maintaining healthy ecosystem and for proper socio-economic development. With increase in population the demand of water for domestic, agriculture and industrial purpose, is also increasing. Over lifting of ground water is creating excessive pressure on the environment [1,2]. Also with the exponentially increasing population pressure huge amount of waste water is being generated. That is why wastewater treatment systems have drawn the interest of scientists in recent years [2,3].

As the waste water collected from various sources is contaminated, it should be treated so as to remove contaminants in order to be released again into their origin [4]. The treatment must remove pathogens, **BOD materials**, excessive nutrients and toxic chemicals [4].

This paper focuses on the determination of BOD rate constant which is very crucial to know the nature of waste water which is discharged into a stream or any other water body [5]. The discharged waste water may severely affect the dissolved oxygen value of the stream or the water body that contains living system [5].

Self-purification of polluted streams or water bodies is affected by the kinetics of deoxygenation and reoxygenation [6]. Information on the oxygen-depleting characteristics of waste water can be

obtained from the BOD reaction kinetics [5,7]. On the other hand this information can be utilized to design the waste water treatment plant [5,8].

2. BOD REACTION:

The simplified representation [4] of aerobic decomposition of organic matter can be given as

Organic matter + O_2 microorganism Products

It is to be noted that our discussion and mathematical formulation regarding BOD is solely due to carbonaceous biochemical oxygen (CBOD) demand and not nitrogenous biochemical oxygen demand (NBOD) which involves oxygen needed to convert biochemical ammonia to nitrate [4]. The reason being, NBOD does not normally begin for the initial five to eight days [7].

3. BOD EQUATION:

The reaction will be considered here as a first order kinetics, so the equation is:

$$y_t = L (1 - e^{-kt}) \dots \dots \dots (1)$$

y_t = the BOD consumed (mg/L) after time t.

L = the ultimate first stage BOD (mg/L)

k = the rate constant

t = time in days

Equation (1) could be written as

$y_{t+h} = L[1 - e^{-k(t+h)}]$ where $h = 1$ day

Or, $y_{t+h} = L [1 - (e^{-kt} \times e^{-kh})]$ (2)

Substituting the value of e^{-kt} from equation (1) to equation (2), we have

$y_{t+h} = L [1 - (L - y_t)/L \cdot e^{-kh}]$

or, $y_{t+h} = L [1 - e^{-kh}] + y_t \times e^{-kh}$ (3)

Equation (3) could be rewritten as a straight line equation

$y_{t+h} = y_t \times e^{-kh} + L [1 - e^{-kh}]$

Where: $L [1 - e^{-kh}] =$ intercept of the line

$e^{-kh} =$ slope of the line

4. SOLUTION FOR K AND L [FUJIMOTO GRAPHICAL METHOD TO FIND UBOD (L)]:

y_{t+h} was plotted against y_t with the help of Microsoft Excel to solve the slope and intercept of the line and hence for K and L.

5. METHODOLOGY:

5.1. SAMPLE COLLECTION

The municipal waste water samples considered in this work were collected from two different sources (1-2 km apart from each other) of Tarapith a small temple town near Rampurhat in Birbhum district of the Indian state of West Bengal.

Out of two waste- water samples, one named as ‘S-A’ was collected 1 to 2 Km apart from main temple area and other sample named as ‘S-B’ was collected from the main temple area of the above mentioned place of Tarapith.

The samples were collected in plastic containers previously cleaned by washing in detergent, followed by rinsing with tap water and finally rinsed with deionized water. During sampling, sample bottles were rinsed with sample water and then filled up to the brim and stored in the refrigerator [9]. Within couple of week the samples were analyzed in SDET-Brainware Group of Institutions, Barasat campus, chemistry/environmental engineering laboratory.

5.2. DETERMINATION OF PARAMETERS

In the present analysis, different parameters e.g. temperature, pH, TSS, COD were determined. Temperature was determined using Celsius thermometer. pH was determined using pH

meter(Systronics-335).COD was determined by using closed reflux method [8].

Chemical oxygen demand (COD):

Chemical oxygen demand is the amount of oxygen consumed by chemically oxidisable organic matter present in the water samples[10]. It is an important variable for characterizing any type of water bodies [1].

COD mg/lit =

Where,

A = volume (ml) of ferrous ammonium sulphate for blank

B = volume (ml) of ferrous ammonium sulphate for sample

N = normality of ferrous ammonium sulphate

V = volume of sample taken

Total suspended solid (TSS):

100 ml of each waste water sample was filtered through pre weighted filter paper (Whatman2).Then the paper was dried at 102-105 °C in hot air oven. Then was cooled in room temperature and weight was taken. From the difference of weight TSS was determined.

5.3. DETERMINATION OF DO AND BOD

Both the samples S-A and S-B were diluted 150 times and diluted samples S-A and S-B individually were transferred to 18 numbers of BOD bottles. Three bottles for each sample were analyzed for Do on the initial day and rest bottles were kept in BOD incubator at 20°C after adding nutrients and phosphate buffer (to maintain the pH at 5.8 ± 0.2).On each subsequent day three bottles corresponding to each sample were tested for DO. This was run for five consecutive days. By subtracting initial DO value from the DO value of a particular day and multiplying by the dilution factor BOD1 to BOD5 were determined. The Winkler azide modification was used for the determination of the DO[9].

Table1. Average BOD Value(mg/lit) For ‘S-A’ And ‘S-B’

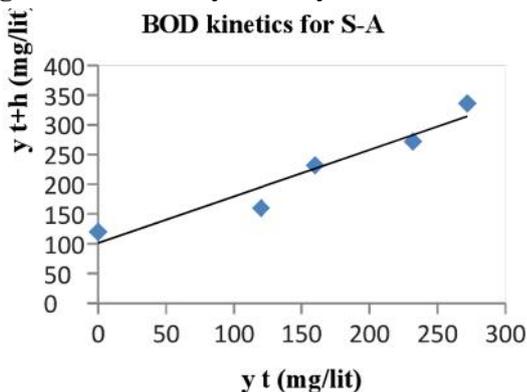
| Sampl e | BOD ₁ | BOD ₂ | BOD ₃ | BOD ₄ | BOD ₅ |
|---------|------------------|------------------|------------------|------------------|------------------|
| S-A | 120 | 160 | 232 | 272 | 336 |
| S-B | 96 | 224 | 280 | 344 | 416 |

To solve BOD rate constant (K) and ultimate BOD (L) equation (3) was considered. y_t and y_{t+h} were also calculated from the same.

Table2. y_{t+h} and y_t for 'S-A'

| Sample | y_t (mg/lit) | y_{t+h} (mg/lit) |
|--------|----------------|--------------------|
| S-A | 0 | 120 |
| | 120 | 160 |
| | 160 | 232 |
| | 232 | 272 |
| | 272 | 336 |

Fig.1. Variation of y_{t+h} with y_t for 'S-A'



From the **fig.1** we have

Slope = $e^{-kh} = 0.7844$ and hence **K = 0.2428 day⁻¹**

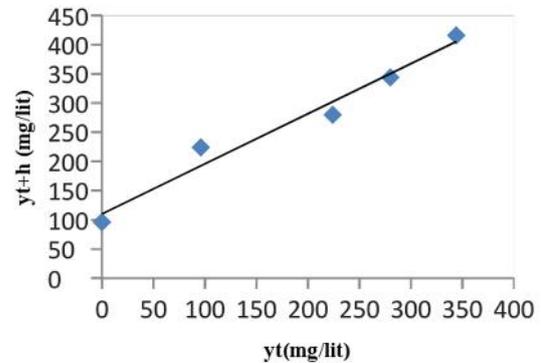
Intercept = $L [1 - e^{-kh}] = 101.01$ and hence

L = 468.506 mg/lit (h = 1)

Table3. y_{t+h} and y_t for 'S-B'

| Sample | y_t (mg/lit) | y_{t+h} (mg/lit) |
|--------|----------------|--------------------|
| S-B | 0 | 96 |
| | 96 | 224 |
| | 224 | 280 |
| | 280 | 344 |
| | 344 | 416 |

Fig.2. Variation of y_{t+h} with y_t for 'S-B'
BOD kinetics for S-B



From the **fig.2**, we have

Slope = $e^{-kh} = 0.8505$ and hence **K = 0.1525 day⁻¹**

Intercept = $L [1 - e^{-kh}] = 109.91$ and hence

L = 776.74 mg/lit (h = 1)

Table4. Comparative study of K_1 and L for S-A and S-B

| Sample | K_1 (day ⁻¹) | L(mg/lit) |
|--------|----------------------------|-----------|
| S-A | 0.2428 | 468.506 |
| S-B | 0.1525 | 776.74 |

6. RESULTS AND DISCUSSIONS:

6.1 TEMPERATURE

Temperature of both S-A and S-B were noted at 30.2 ± 2 after sample collection.

6.2 pH

pH of S-A was noted at 4.43 and of S-B was noted at 4.88, which are much lower than the limits (5.5-9.0) set by Indian Standards. It may be due to the decomposition of food ingredients that form acid.

6.3 BOD & COD

The biological oxygen demand for five days at 20°C (BOD₅) and chemical oxygen demand (COD) levels were normal[5].

6.4 TSS

Amount of total suspended solid (TSS) for both S-A and S-B were not within the limits (100 mg/lit) set by Indian Standards.

6.5 BOD reaction rate constant(K_1)

Our result for K_1 (**Table4**) was found to be closer to that reported by F.M. Abdelrasoul et al., 1996[5]

Table5. Physicochemical parameters for S-A and S-B done by us

| Sample | pH | TSS mg/lit | BOD5 mg/lit | COD mg/lit |
|--------|-----|---------------|----------------|---------------|
| S-A | 4.4 | 370 | 336 | 688.45 |
| S-B | 4.8 | 150 | 416 | 966 |

Table6. Physicochemical parameters for Rakta and Sewage Sample done by F.M. Abdelrasoul 1996[5]

| Sample | pH | TSS mg/lit | BOD5 mg/lit | COD mg/lit |
|--------|-----|---------------|----------------|---------------|
| Rakta | 8.1 | 825 | 487.2 | 1200 |
| Sewage | 7.4 | 243 | 174.5 | 400 |

8. Conclusions:

The rate constant K_1 of the BOD reaction for the two municipal waste water samples were determined for a 20°C .

It is seen that the waste water samples S-A having lower value of ultimate BOD value has higher rate of reaction whereas the sample S-B having higher value of ultimate BOD has reaction rate lower. This may due to the presence of some organic compounds in the sample S-B which are not easily biodegradable but ultimately degrades

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